





Distributed Generation Improvements in Industrial Applications

CHP Integration with Fluid Heating Processes in the Chemical and Refining Sectors

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CHP Integration with Fluid Heating in Chemical and Refining Sectors

- Links to DER Strategy
 - Encourage CHP in Industry (Chemical and Refining)
 - Incremental Fluid Heating CHP Applications Could Double the CHP Potential from Traditional Steam Systems
 - Environmental and Efficiency Benefits

Impact to CHP Opportunity in Chemical and Refining Sectors

- Based on Selected Chemicals and Refining Processes
- 22 GW of Remaining New Steam CHP Potential
- 44 GW of New Fluid Heating CHP Potential
- 66 GW of Total New CHP Potential

(7 GW of Existing CHP Capacity in Selected SICs)

CHP Integration with Fluid Heating in Chemical and Refining Sectors

Objectives

- Estimate the MW Potential of a Larger CHP Market as Compared to Traditional Steam CHP
- Evaluate Technical Issues Including Temperature Requirements and Process Integration
- Industrial Survey to Augment Field Findings
- Recommendations to Overcome Economic and Technical Hurdles

Scope of Work

PROGRESS	•	Task 1: Market Assessment			
Completed		 Identify SICs with fluid heating processes, equipment types, temperatures 			
		 Estimate MW potential, develop economic criteria for U.S. 			
	•	Task 2: Technical Feasibility			
		 Detailed evaluation of two fluid heating applications (ethylene plant and refinery) 			
In progress		 Investigate issues affecting feasibility of CHP integration (economic & environmental) 			
	•	Task 3: Industrial Survey			
		 Discussion Paper 			
		Perform Industrial Survey			
TBD		Recommendations			
	•	Task 4: Final Report			

Task 1.1 - Fluid Heating Processes

Refining Processes	Fluid Heating CHP (GW)	Chemical Processes	Fluid Heating CHP (GW)
Distillation		Ethylene	5.50
Atmospheric	10	Ammonia	1.9
Vacuum	3	Carbon Black	0.57
Vaddiii	O	Methanol	0.48
Coking	4	Urea	0.27
Catalytic Processes		Styrene	0.24
•	0	Vinyl Chloride	0.22
Fluid Cracking	3	Benzene, Toulene, Xylenes	0.18
Reforming Hydrocracking	8	Soda Ash	0.08
	2	Propylene Oxide	0.08
Hydrotreating	5	Propylene Oxide	0.08
		Caprolactam	0.05
Total	34	Acrylonitrile	0.01
		Total	9.66

Task 1.2 & 1.3 - Target Markets

Regions with Positive "CHP Spark Spread"

- Texas (14 GW)
- Louisiana (7.8 GW)
- California (4.8 GW)
- Pennsylvania (1.3 GW)
- New Jersey (1.2 GW)
- Washington (1.2 GW)
- Minnesota (0.7 GW)
- Note: "CHP spark spread" is defined as average industrial electric price compared to cost of power from a 5MW CHP system including fuel, capital and O&M

Task 2.1 - Technical Assessment

- Direct-Coupled CHP (e.g. ethylene plant example)
 - Gas Turbine Exhaust Used as Combustion Air to Furnace
 - Can be integrated with all process temperature requirements
 - Gas turbine selection based on mass flow through furnace
 - Design sensitive to exhaust O₂ content and temperature
 - Gas turbines with lower inlet temperatures with higher O₂
 preferred
 - Single shaft turbines exhibit favorable thermal inertia characteristics in the case of an emergency shut-down

Task 2.1 - Technical Assessment

- Indirect-Coupled CHP (e.g. Paramount Refinery)
 - Gas turbine exhaust is directed to a waste heat exchanger (no fluid mixing)
 - Well suited to convection heat transfer applications (no-high temperature radiant duty)
 - Not suitable for processes with high-temp endothermic "cracking" chemical reactions
 - Fluid heating and steam generation can be accomplished in a single waste heat exchanger

Progress to Date

Progress Report Submitted

- Task 1: Fluid Heating Market
 - Identify SICs with Fluid Heating (Task 1.1)
 - Database Screening (Task 1.1)
 - Economic Criteria (Task 1.2)
 - Target Markets (Task 1.3)
- Task 2: Site Evaluation
 - Performed Refinery Site Visit (Task 2.1)
 - Performed Technical Assessment (Task 2.1)
 - Economic and Environmental Assessment (Task 2.2)
 - Recommendations (Task 2.3)
- Task 3: Industrial Survey
 - Discussion Paper (Task 3.1)
 - Perform Industrial Survey (Task 3.2)
 - Recommendations (Task 3.3)
- Task 4: Final Report

Schedule

